# Solving time-dependent PDEs using the material point method, a case study from gas dynamics

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#### **SUMMARY**

The material point method (MPM) developed by Sulsky and colleagues is currently being used to solve many challenging problems involving large deformations and/or fragementations with some success. In order to understand the properties of this method, an analysis of the considerable computational properties of MPM is undertaken in the context of model problems from gas dynamics. The MPM method in the form used here is shown both theoretically and computationally to have first-order accuracy for a standard gas dynamics test problem. Copyright © 2009 John Wiley & Sons, Ltd.

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#### 1. INTRODUCTION

The need to solve problems involving large deformations in materials has led to the development of a number of new computational methods. Examples of such methods are meshfree and particle methods, for example, as surveyed by Li and Liu [1], one of which is the relatively new material point method (MPM) of Sulsky *et al.* [2, 3], which may, perhaps, be described as a quasi-meshless method. This method (MPM) has evolved from the particle-in-cell (PIC) and FLIP methods [4] originally developed by Brackbill see [5] and the references within. An interesting discussion

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of some of these methods and important theoretical results are given by Grigoryev *et al.* [6]. Two important features of MPM are the use of a grid as a scratchpad for calculations, hence the quasi-meshless characterization and the capability to model solid materials undergoing large deformation. An important aspect of the MPM method is that it has not yet been subjected to as much analysis as many of the methods surveyed by Li and Liu [1].

There has been considerable analysis of PIC type methods. One of the fundamental aspects of PIC methods is a discretization of a material into particles, and the interpolation of information from particles to grids and vice versa. In MPM, Lagrangian particles (or points) are used to discretize the volume of the fluid or solid. These material points carry with them the properties such as mass, velocity, stress, strain and so on. The grid may be viewed as a temporary computational scratch pad, which can be reconnected at any time when a mesh distortion makes further calculation more difficult. Material response is governed by continuum mechanics constitutive models, which generates stress based on both the history and current mechanical states, [2]. The generalized interpolation material point method (GIMP) [7] provides a general formulation covering MPM methods. MPM has been used for applications such as the biomechanics of micro-vessels, the effects of wounding on heart tissue and the properties of foam under large deformation [8]. The method has also been used extensively in large-scale complex fluid–structure interactions [9, 10], arising from the modeling of safety studies involving explosions. Given the use of the method on such important and challenging problems, it is important to understand how accurate the method is.

In this paper, an analysis of the MPM procedure is considered in the context of a shock propagation problem, using a modified form of the method developed by Kim [11]. This problem has also been studied by Burgess *et al.* [12], Sulsky *et al.* [2], York *et al.* [13] and very recently in the context of SPH methods by Brownlee *et al.* [14]. A comparison between MPM and the SPH method has been undertaken by Ma *et al.* [15]. Although MPM is originally designed for solid mechanics problems, this test problem has the advantage of being sufficiently simple and well-understood to allow analysis of the method. Furthermore, the problem's analytical solution can be used to evaluate the various sources of error in the MPM method. This paper describes the accuracy and stability properties of the MPM method in a way that also allows these properties to be extended to other more general situations. A particular focus of the paper is an analysis of different methods used to project information from particles onto the grid. The errors introduced when the particles cross grid cells are also studied in some depth. The paper is complementary to other recent studies of the method [16–19].

## 2. PROBLEM DESCRIPTION

The model problem used here is that of Sod [20] who used a simple gas dynamics problem to investigate finite difference schemes for shock propagation type problems. This problem has an analytical solution and may be used to compare the result of MPM with the analytical solution. The same problem has often been used as a test problem for PIC and MPM methods [13].

Sod's gas dynamics problem consists of a shock tube, where a diaphragm is located in the middle of the tube. Two sides of the diaphragm have different pressures and densities, which make the fluid flows when the diaphragm is broken. The left side of density is 1 and pressure is also 1. The right side of density is 0.125 and pressure is 0.1, and the initial velocities of both regions are zero. At time t = 0, the diaphragm is removed, the motion of the compressible and inviscid fluid

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is governed by Euler's equations, which are,

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho v}{\partial x} = 0$$

$$\frac{\partial \rho v}{\partial t} + \frac{\partial (\rho v^2 + p)}{\partial x} = 0$$

$$\frac{\partial \rho e}{\partial t} + \frac{\partial v(\rho e + p)}{\partial x} = 0$$
(1)

where e is the total energy per unit volume, p the pressure, v the unit velocity,  $\rho$  the fluid density and  $(x,t)\varepsilon(0,1)\times(0,0.1)$ . The state equation for pressure is

$$p = (\gamma - 1) \left( \rho e - \frac{\rho v^2}{2} \right) \tag{2}$$

where  $\gamma = 1.4$  denotes the ratio of specific heat for dry air as a perfect gas. These equations may be written, e.g. using Equations 14.45–14.47 of [21] in the form given by Sulsky *et al.* [2] as

$$\frac{\partial \varepsilon}{\partial t} + v \frac{\partial \varepsilon}{\partial x} + \frac{p}{\rho} \frac{\partial v}{\partial x} = 0 \tag{3}$$

$$\frac{\partial \rho}{\partial t} + v \frac{\partial \rho}{\partial x} + \rho \frac{\partial v}{\partial x} = 0 \tag{4}$$

where  $\varepsilon$  denotes the internal energy. The state equation for pressure is then given by:

$$p = (\gamma - 1)\rho\varepsilon \tag{5}$$

The boundary conditions are those commonly used [20].

#### 3. MPM SPATIAL DISCRETIZATION

## 3.1. Particle basis functions

The original form of the MPM method uses Delta functions for the basis functions associated with the *np* particles

$$\chi_p(x) = \delta(x - x_p)V_p, \quad p = 1, \dots, np$$
(6)

where  $x_p(t)$  are particle positions which are functions of time t and  $V_p$  is a particle volume that is discussed below. Bardenhagen and Kober [7] use the piecewise constant form instead

$$\chi_p(x) = \begin{cases} 1 & \text{if } x \in \Omega_p \\ 0 & \text{otherwise} \end{cases}$$
 (7)

where  $\Omega_p$  is the interval  $[x_p - h_p/2, x_p + h_p/2]$  and  $h_p$  is the particle width. This has the advantage that the functions form a partition of unity on the interval [a, b]:

$$\sum_{p=1}^{np} \chi_p(x) = 1 \quad \forall x \in [a, b]$$

$$\tag{8}$$

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For both choices of basis functions, the approximation to the function f(x) in terms of particle values is then written as

$$f(x) \approx \sum_{p} f_p \chi_p(x) \quad \forall x \in [a, b]$$
 (9)

The particle volumes are then defined by

$$V_p = \int_{\mathcal{O}^i} \chi_p(x) \, \mathrm{d}x \tag{10}$$

where  $\Omega^i$  is the domain of cell *i* that contains the particle *p*. In the case when  $\chi_p(x)$  is defined as by Equation (6) the 'volume' of a particle will be defined in Section 5 below.

# 3.2. Grid basis functions

The continuous representation of a function g(x) using grid data  $g_i$  on a grid

$$a = x_0 < x_1 < \dots < x_N = b$$
 (11)

and where  $I_i = [x_{i-1}, x_i]$  and  $I_{i+1} = [x_i, x_{i+1}]$  and  $h_i = x_i - x_{i-1}$  is given by

$$g(x) = \sum_{i=1}^{n_v} g_i S_i(x)$$
 (12)

where  $S_i(x)$  is the piecewise linear basis function with value one at node  $x_i$  in the mesh and value zero at all other nodes; often these points are equidistant with an uniform mesh spacing of h.

## 3.3. Mapping from particles to grid

The mapping from particle values to values at grid points is defined by the convolution of the linear basis functions or their gradients with the particle basis functions as follows. Let

$$\bar{S}_{ip} = \frac{1}{V_p} \int_{\Omega^i} S_i(x) \chi_p(x) \, \mathrm{d}x \tag{13}$$

and

$$\bar{G}_{ip} = \frac{1}{V_p} \int_{\Omega^i} \frac{\mathrm{d}S_i}{\mathrm{d}x}(x) \chi_p(x) \,\mathrm{d}x \tag{14}$$

In the case of the standard MPM case when delta functions are used for the particles and linear basis functions are used for the grid, then [7],

$$\bar{S}_{ip} = S_i(x_p) \tag{15}$$

and

$$\bar{G}_{ip} = \frac{\mathrm{d}S_i}{\mathrm{d}x}(x_p) \tag{16}$$

The mapping from particle values to values at grid points is then defined by

$$f(x_i) = \sum_{p=1}^{np} f(x_p) \bar{S}_{ip}$$
 (17)

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## 4. COMPUTATIONAL METHOD

Given an initial distribution of particles on the domain, the point masses,  $m_p$ , are defined in terms of density by:

$$m_p = \int_{\Omega^i} \rho(x) \chi_p(x) \, \mathrm{d}x \tag{18}$$

A point density average,  $\rho_p$ , may also be defined by

$$\rho_p = m_p / V_p \tag{19}$$

Particle momentum values,  $P_p$ , are given by

$$P_p = \int_{\Omega^i} \rho(x) v(x) \chi_p(x) \, \mathrm{d}x \tag{20}$$

where  $\rho(x)$  is the continuum body's mass density and v(x) is the velocity.

The Cauchy stresses are

$$\sigma_p = \int_{\Omega^i} \sigma(x) \frac{\chi_p(x)}{V_p(x)} dx \tag{21}$$

where  $\sigma(x)$  is continuum bodies initial Cauchy stress. In the most general case, the stress tensor is given by  $\sigma = -pI + T$ , where p is the pressure, T denotes the viscous stress tensor and I is an identity tensor whose size is the same as the modeling dimension. In a perfect fluid model such as the gas dynamics problem considered here, the stress at a particle is equal to the pressure:

$$\sigma_p = -p_p \tag{22}$$

## 4.1. Mesh and particle movement per time step

This subsection is an abbreviated form of the description of the MPM method in [17]. At the start of a time step, the mass at each grid point,  $m_i$ , is calculated from the masses of the particles, by using the lumped mass matrix form of MPM [2]:

$$m_i = \sum_{p=1}^{np} \bar{S}_{ip} m_p, \quad i = 1, ..., nv$$
 (23)

where nv is the number of nodes. Momentum at a grid node,  $P_i$ , is given by

$$P_{i} = \sum_{p=1}^{n_{p}} \bar{S}_{ip} m_{p} v_{p}, \quad i = 1, \dots, nv$$
 (24)

The nodal velocity,  $v_i$ , is calculated from the mass and the momentum of the node:

$$v_i = \frac{P_i}{m_i} \tag{25}$$

The force at each node,  $F_i^{int}$ , is given by

$$F_i^{\text{int}} = \sum_{p=1}^{np} p_p \bar{G}_{ip} V_p \tag{26}$$

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where  $p_p$  is the particle pressure. The acceleration at a node,  $a_i$ , is calculated from the force and the mass at the node:

$$a_i = \frac{F_i^{\text{int}}}{m_i} \tag{27}$$

The nodal velocity at the end of Lagrangian step is calculated using Euler's method

$$v_i^{n+1} = v_i^n + a_i^n \,\mathrm{d}t\tag{28}$$

where  $a_i^n$  is the acceleration at time  $t_n$ . The particle velocity and location are updated using these new values:

$$v_p^{n+1} = v_p^n + \sum_{i=1}^{n_v} \bar{S}_{ip} a_i^n dt$$
 (29)

$$x_p^{n+1} = x_p^n + \sum_{i=1}^{n_v} \bar{S}_{ip} v_i^{n+1} dt$$
 (30)

Remark

If  $v_p^{n+1}$  was used to replace the sum in the right side of Equation (30), the time integration method could be viewed as a first-order Runge–Kutta–Nystrom method [22].

#### 5. APPLICATION TO GAS DYNAMICS

At the start of a time step, the approximate particle volume for particle p can be calculated from the width of the cell it lies in,  $h_j$ , and the number of particles in that cell,  $N_p^j$ , by

$$V_p = \frac{h_j}{N_p^j} \tag{31}$$

while this is a reasonable approximation for compressible flow, and was first used by Kim [11], it represents a departure from the standard MPM approach for solid mechanics, in which the volumes associated with particles are tracked, see [16], for an analysis of this case. The particle's mass is calculated from the density and the volume of the particle as

$$m_p = \rho_p V_p \tag{32}$$

The mass at each grid point is calculated from the projection of the particle properties as in (23) and the momentum at a grid node is given by Equation (24). The nodal velocity is calculated from the mass and the momentum of the node as given in (25). The force at each node may be written as the jump on the averaged particle pressures

$$F_i^{\text{int}} = p_{p,i}^- - p_{p,i}^+ \tag{33}$$

where

$$p_{p,i}^{-} = \sum_{p:x_p \in I_i} p_p \frac{1}{N_p^i}$$
 (34)

$$p_{p,i}^{+} = \sum_{p:x_p \in I_{i+1}} p_p \frac{1}{N_p^{i+1}}$$
(35)

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The internal force at a node is thus equal to the averaged pressure drop around that node. The acceleration at a node is calculated from the force and the mass at the node

$$a_i = \frac{p_{p,i}^- - p_{p,i}^+}{m_i} \tag{36}$$

The particle velocity and location are updated using these values by Equations (28)–(30). This method of force calculation has been developed here as being more appropriate for compressible gas dynamics as it assumes that the particles within a cell have the same volume. Analysis and investigation of alternative methods for solid mechanics and different approaches to gas dynamics are provided by [6, 13, 16].

## 5.1. Particle energy, density and pressure update

Once the nodal velocities are known as in Equation (29), it is possible to update the velocity gradient and hence calculate the energy and a density of the particles at the next time step, as denoted by  $\varepsilon_p^{n+1}$ ,  $\rho_p^{n+1}$  by

$$\varepsilon_p^{n+1} = \varepsilon_p^n - \frac{p_p^n}{\rho_p^n} \frac{\partial v_p^{n+1}}{\partial x} dt$$
 (37)

and

$$\rho_p^{n+1} = \rho_p^n \left( 1 - \frac{\partial v_p^{n+1}}{\partial x} \, \mathrm{d}t \right) \tag{38}$$

where the velocity gradient of each particle is calculated using nodal velocities and the gradients of the nodal basis functions by using

$$\frac{\partial v_p^{n+1}}{\partial x} = \sum_{i=1}^{nv} \bar{G}_{ip} v_i^{n+1}$$

where  $\bar{G}_{ip}$  is defined by equation (14). The pressure update is given by:

$$p_p^{n+1} = (\gamma - 1)\rho_p^{n+1} \varepsilon_p^{n+1} + a_v \tag{39}$$

The term  $a_v$  is a standard artificial viscosity term which is defined by

$$a_v^n = \begin{cases} C^2 dx^2 \rho \left(\frac{\partial v_p}{\partial x}\right)^2 & \text{if } \frac{\partial v_p}{\partial x} \leq 0\\ 0 & \text{otherwise} \end{cases}$$

where C = 2.5. This form of artificial viscosity was used by Monaghan and Gingold, and Monaghan and Pongracic [23, 24] to reduce oscillations in the numerical solution SPH methods. This formula exploits the property of shock front that the gradient of velocity is less than zero, there. Using the pressure Equation (5) to substitute for the pressure/density ratio in the energy equation gives:

$$\varepsilon_p^{n+1} = \varepsilon_p^n \left( 1 - (\gamma - 1) \frac{\partial v_p^{n+1}}{\partial x} dt \right) - \frac{a_v}{\rho_p^n} \frac{\partial v_p^{n+1}}{\partial x} dt \tag{40}$$

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In the same way the pressure Equation (5) may itself be rewritten as:

$$p_p^{n+1} = \left[ (p_p^n - a_v^{n-1}) \left( 1 - \frac{\partial v_p}{\partial x} dt \right) + a_v^n \right] \left( 1 - (\gamma - 1) \frac{\partial v_p^{n+1}}{\partial x} dt \right)$$
(41)

# 5.2. Positivity, overshoots and stability

As density, energy and pressure values are positive, their numerical approximations should also be positive. From Equations (37)–(38) it may be seen that this occurs for the discrete density and energy equations under a Courant-like condition:

$$0 \leqslant \frac{\partial v_p^{n+1}}{\partial x} \, \mathrm{d}t \leqslant 1 \tag{42}$$

Although this ensures that the values of density and energy remain positive; local extrema may be caused by the use of the velocity gradient from 'old' cell when cell crossing occurs. Suppose that there are two adjacent particles in different mesh intervals with densities,  $\rho_p$  and  $\rho_{p+1}$ . Suppose further that

$$\rho_p(t_n) < \rho_{p+1}(t_n) \tag{43}$$

and that the velocity gradients  $\partial v_p/\partial x$  differ in adjacent intervals so that

$$\left(1 - \mathrm{d}t \frac{\partial v_p^{n+1}(x_p)}{\partial x}\right) \gg \left(1 - \mathrm{d}t \frac{\partial v_p^{n+1}(x_{p+1})}{\partial x}\right) \tag{44}$$

then it is possible that one particle will over take the other in magnitude:

$$\rho_{n}(t_{n+1}) > \rho_{n+1}(t_{n+1}) \tag{45}$$

this may result in a new extremal value. A similar argument may be developed for the creation of new extrema in energy. In order to prevent this further artificial diffusion is applied in the case when extrema occur in velocity  $(v_{i-1}-v_i)(v_{i+1}-v_i)>0$ . The new value of velocity is then calculated by the addition of an artificial viscosity-like term that approximates  $(h_i^2/3)(\partial^2 v/\partial x^2)$  gives

$$v_i = v_i + \frac{v_{i-1} - 2v_i + v_{i+1}}{3} \tag{46}$$

and the same approach is applied if extrema are detected in density.

#### 5.3. Particle redistribution

Once particles move to an adjacent cell, the changed number of particles in a cell is used to calculate new particle volume and mass after the density calculation is completed. If there were too few particles per cell and some of these particles move from one cell to another cell, it is possible for a cell not to have any particles. This may cause stability problems. To prevent this situation, care must be taken in the initial assignment of particles, see Section 6.1. The main idea is to ensure that there are always sufficient number of particles per cell. This may be obtained by redistributing particles or by ensuring that particles are placed where they will move into cells

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with less particles. It may also be necessary to create new particles in the empty cells with the particles' properties obtained by interpolating the particles' properties in the adjacent cells.

#### 6. GAS DYNAMICS COMPUTATIONAL EXPERIMENTS

## 6.1. Initial uniform particle distribution

In these experiments the spatial mesh is fixed, and as particles can move from one cell to another cell, the number of particles in a cell varies, and so does their volume according to Equation (31). Since we assume that each material point is a part of a perfect compressible gas, changing the particle's volume is a reasonable modeling assumption. Initially, same number of particles per a cell is used. Figures 1(a), (b) are the results after 0.2 s. The initial number of particles in a cell is eight, the cell size is 0.005 and time step is 0.00025. Each dot represents a material point and a solid line is the analytical solution.

Figures 1(a), (b) show large errors behind the shock front. The smoothing process described in Section 5.2 was applied to density and velocity as a remedy for this. Figures 2(a), (b) show the solution after the smoothing process was applied. The error norm after the smoothing process is about 67–90% of that when smoothing is not applied.

In investigating the relationship between the error and cell size, number of particles and time interval, a smaller cell size generated more accurate results. When the number of particles is too small (1, 2 or 3), the computation was inaccurate or unstable no matter how small the cell size was. When the number of particles in a cell was between 4 and 8 and a sufficiently small cell size was used the best results were obtained. In addition it is interesting to see that the smaller cell size does not reduce the need for a certain number of particles in a cell in order for a stable and accurate result to be obtained. Smaller time steps generated slightly better results at the cost of increased calculation times. The conclusion thus is that between 4 and 8 particles should be used in this situation with this method. Section 6.2 will show that this may be modified based on the difference of density in various regions.

Figure 3(a) shows the final L2 error norms with a fixed time interval but different cell sizes and shows that the L2 norm is decreasing as the cell size decreases. The figure also shows that

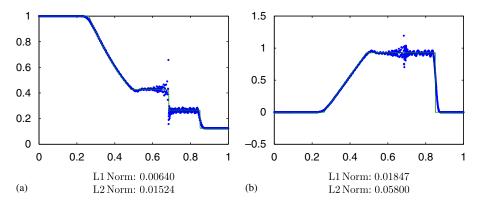


Figure 1. (a) Density error and (b) velocity error.

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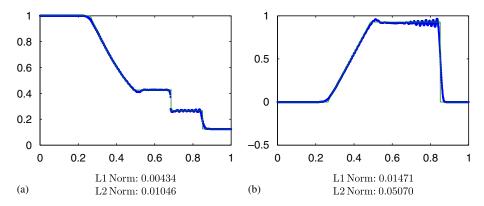


Figure 2. (a) Density error and (b) velocity error.

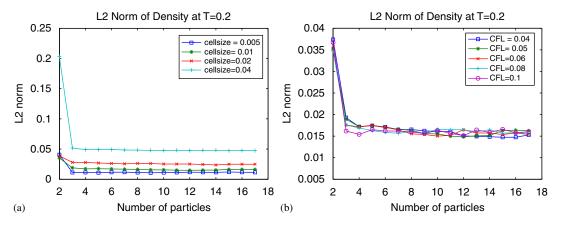


Figure 3. (a) Error vs cell size and (b) error vs CFL number.

the number of particles is not the main factor for a smaller error norm if the number of particles is not too small. Figure 3(b) shows that for the same cell size but different time steps the error did not change much for CFL numbers below 0.1. Figure 3(b) shows slightly increasing errors as the time interval decreases, perhaps due to error buildup over the larger number of steps, but overall the spatial error dominates the temporal error. In order to investigate stability and choice of CFL number, two test cases were used. First of all, cell size and the number of particles per cell were fixed, and time interval is changed. When the cell size was 0.005, the modeling system was unstable if the time interval was bigger than 0.00057. The meaning of 'unstable' is that the particle's velocity was so large that the particle left the spatial domain. Table I shows that the method generates stable results only if the CFL number is smaller than about 0.11–0.12, and the smoothing process allows a slightly larger CFL number than the non-smoothing process does.

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	0.005		0.01		0.015	
Cell size (dX)	N.S.*	S*	N.S.	S	N.S.	S
Max stable time step (dt) Max stable CFL(dT/dX)	0.00057 0.114	0.0006 0.124	0.00114 0.114	0.00124 0.124	0.00171 0.114	0.00185 0.123

Table I. Values of stable time step size.

<sup>\*</sup>NS: non-smoothing process, S: smoothing process applied.

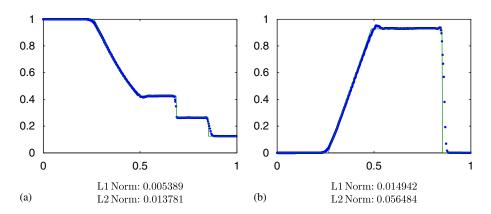


Figure 4. (a) Density and (b) velocity.

#### 6.2. Alternative particle distribution

Although the smoothing process reduced much of instability of the particles, there are still remaining spurious oscillations in the solution. Brackbill [25] showed that the ringing instability in the PIC method was reduced with smaller number of particles, see Section 8. This result suggests using a smaller number of particles. However, using (2-3 particles) increases error and one particle in a cell may generate unstable results. This problem is overcome by noting that, based on the given initial condition, the gas to the right of the diaphragm has a lower density. Hence, particles are assigned in proportion to the relative density of the gasses. Since the gas on the left side has normalized density 1 and that on the right has density 0.125, eight particles per a cell are assigned to the left and one particle to the right. Interestingly, this particle distribution gives a stable result although the number of particles on the right side is one per cell. During the time integration process, the left particles move rightwards. As there are enough number of particles on the left side and these particles move to the right where there is only one particle per cell, the solution process remains stable as we are constantly introducing particles into the cells on the right. Figures 4(a), (b) show the results from using fewer particles on the right-hand side of the diaphram. The Smoothing process of Section 5.2 was also applied. Comparing these images with Figures 2(a), (b), this approach results in fewer oscillations, but has a similar error norm to the previous cases. A generalization of this approach is to equally distribute particles with respect to density.

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## 7. TIME INTEGRATION ERROR AND GRID CROSSING BY PARTICLES

# 7.1. Time integration discontinuities arising from grid crossing

The comparative lack of smoothness of the spatial basis grid functions used in the MPM translates into a lack of smoothness in time when particles cross grid points and then have properties that are redefined in terms of the basis functions in the next interval. The definition of particle velocity updates in terms of nodal velocity values means that the higher time derivatives of the particle velocity are discontinuous when a particle crosses a grid point. This may be illustrated by considering Equation (28), which is a forward Euler discretization of

$$\dot{v}_p = \sum_i S_i(x_p) a_i \tag{47}$$

If the point  $x_p(t)$  is in the interval  $[x_{i-1}, x_i]$  then this equation may be written as

$$\dot{v}_p = \alpha_i a_{i-1} + (1 - \alpha_i) a_i, \quad \alpha_i = \frac{x_p(t) - x_i}{x_{i-1} - x_i}$$
(48)

whereas if the point  $x_p(t)$  is in the interval  $[x_i, x_{i+1}]$  then this equation may be written as

$$\dot{v}_p = \alpha_{i+1}a_i + (1 - \alpha_{i+1})a_{i+1}, \quad \alpha_{i+1} = \frac{x_p(t) - x_{i+1}}{x_i - x_{i+1}}$$
(49)

The second derivative of  $v_p$  when the point  $x_p(t)$  is in the interval  $[x_{i-1}, x_i]$  is given by

$$\ddot{v}_p = \alpha_i \dot{a}_{i-1} + (1 - \alpha_i) \dot{a}_i + \dot{x}_p \frac{a_{i-1} - a_i}{x_{i-1} - x_i}$$
(50)

or if the point  $x_p(t)$  is in the interval  $[x_i, x_{i+1}]$  then

$$\ddot{v}_p = \alpha_{i+1}\dot{a}_i + (1 - \alpha_{i+1})\dot{a}_{i+1} + \dot{x}_p \frac{a_i - a_{i+1}}{x_i - x_{i+1}}$$
(51)

The jump in the second derivative of particle velocity as the particle crosses the point  $x_i$  is given by

$$[\ddot{v}_p^+ - \ddot{v}_p^-]_{x_i} = \dot{x}_p \left[ \frac{a_i - a_{i+1}}{x_i - x_{i+1}} - \frac{a_{i-1} - a_i}{x_{i-1} - x_i} \right]$$
 (52)

The local error associated with one step of the forward Euler method applied to Equation (29) is given by

$$le = \frac{\mathrm{d}t_1^2}{2}\ddot{v}_p \tag{53}$$

This formula does not apply if  $\ddot{v}_p$  is discontinuous with 'left' and 'right' values denoted by  $\ddot{v}_p^-$  and  $\ddot{v}_p^+$ , respectively. One standard ODE method for crossing a discontinuity is to march up to it with one step of size  $dt_1$  and one step from it of size  $dt_2$ . The local error for an Euler time step in region one may be estimated by

$$le_1 \approx \frac{\mathrm{d}t_1^2}{2} \ddot{v}_p^- \tag{54}$$

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and the local error for an Euler time step in region two is estimated by

$$le_2 \approx \frac{\mathrm{d}t_2^2}{2} \ddot{v}_p^+ \tag{55}$$

by assuming that the second derivatives may be regarded as constant on a step. It may be shown by using techniques such as those used by Shampine [26] that the error introduced over one time step, denoted here by  $e_p^{p+1}$ , that crosses the discontinuity is then the sum of these local errors and the difference between the one- and two-step solutions, i.e.

$$e_p^{p+1} = le_1 + le_2 + (\bar{v}_p^{n+1} - v_p^{n+1})$$
 (56)

where  $v_p^{n+1}$  is the solution computed using one Euler step of size dt and where  $\bar{v}_p^{n+1}$  is the solution computed using two Euler steps of size  $dt_1$  and  $dt_2$ . The next two sub-sections will show that the gap between the two Euler solutions  $(\bar{v}_p^{n+1} - v_p^{n+1})$  is one power of dt less than the local errors for both velocity and position errors.

# 7.2. Time integration errors in velocity

Having determined the nature of the discontinuity, it now remains to determine the error introduced by stepping over it. In both these cases, the discontinuity in the first time derivative of the right-hand side of Equation (43) (after noting that  $x_p$  is time dependent) means that the time integration method accuracy is restricted to first order unless special action is taken [27, p. 64]. It is worth noting that with a standard p.d.e. method discontinuities in time derivatives do not occur in the same way as when MPM particles cross cells. In the case when a particle  $x_p$  lies in  $I_i$  and passes over a mesh cell (Figure 5) then Figure 6 illustrates the different values of spatial position that may result when the discontinuity is and is not considered.

$$v_p^{n+1} = v_p^n + \left[ a_{i-1} + \frac{x_p^n - x_{i-1}}{x_i - x_{i-1}} (a_i - a_{i-1}) \right] dt$$
 (57)

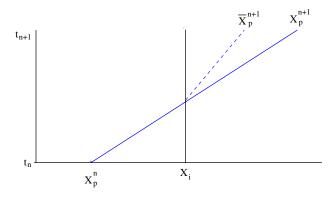


Figure 5. Mesh crossing diagram.

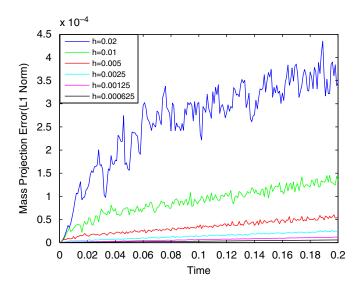


Figure 6. L1 norm of mass errors at nodes for different meshes.

Alternatively, the forward Euler method may be applied to march up to the edge of the cell in one step and then take another step to arrive at the same point. For the first sub step of length  $dt_1$  the velocity is

$$\bar{v}_i = v_p^n + \left[ a_{i-1} + \frac{x_p^n - x_{i-1}}{x_i - x_{i-1}} (a_i - a_{i-1}) \right] dt_1$$
(58)

For the second sub step

$$\bar{v}_{p}^{n+1} = \bar{v}_{i} + [a_{i} + dt_{1}\dot{a}_{i}] dt_{2}$$
(59)

where  $dt = dt_1 + dt_2$ . Hence the difference in the velocities calculated using the two approaches is given by

$$\bar{v}_p^{n+1} - v_p^{n+1} = (a_i - a_{i-1}) \left[ \frac{x_i - x_p^n}{x_i - x_{i-1}} \right] dt_2 + dt_1 dt_2 \dot{a}_i$$
 (60)

and so may be written as

$$\bar{v}_p^{n+1} - v_p^{n+1} \approx C \, dt_2(a_i - a_{i-1}) + \text{H.O.T}$$
 (61)

where  $C = [x_i - x_p^n/x_i - x_{i-1}]$  and where  $0 \le C \le 1$ . For the Euler equations considered here the values of  $(a_i - a_{i-1})$  may be as large as  $10^3$ . This dictates the use of a time step of the order of that used in Section  $6.^{\ddagger}$ 

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 $<sup>^{\</sup>ddagger}$ The reader should note that throughout C will be used as a generic constant whose value may be different each time it is used.

# 7.3. Time integration errors in spatial position

Having determined the nature of the discontinuity, it now remains to determine the error introduced by stepping over it. In both these cases, the discontinuity in the higher derivative means that the time integration method accuracy is again restricted to first order. In the case when a particle  $x_p$ lies in  $I_i$  and passes over a mesh cell then

$$x_p^{n+1} = x_p^n + \left[ v_{i-1}^{n+1} + \frac{x_p^n - x_{i-1}}{x_i - x_{i-1}} (v_i^{n+1} - v_{i-1}^{n+1}) \right] dt$$
 (62)

which may be written as

$$x_p^{n+1} = x_p^n + \left[ v_{i-1}^n + \frac{x_p^n - x_{i-1}}{x_i - x_{i-1}} (v_i^n - v_{i-1}^n) \right] dt + \left[ a_{i-1}^n + \frac{x_p^n - x_{i-1}}{x_i - x_{i-1}} (a_i^n - a_{i-1}^n) \right] dt^2$$
 (63)

As stated above, consider using the forward Euler method to march up to the edge of the cell in one step and then in another step to step to the same time point. For the first step

$$x_{i} = x_{p}^{n} + \left[v_{i-1}^{n} + \frac{x_{p}^{n} - x_{i-1}}{x_{i} - x_{i-1}}(v_{i}^{n} - v_{i-1}^{n})\right] dt_{1} + \left[a_{i-1}^{n} + \frac{x_{p}^{n} - x_{i-1}}{x_{i} - x_{i-1}}(a_{i}^{n} - a_{i-1}^{n})\right] dt_{1}^{2}$$

$$(64)$$

For the second step

$$\bar{x}_p^{n+1} = x_i + v_i^{n+1} dt_2 \tag{65}$$

and so

$$\bar{x}_{n}^{n+1} = x_{i} + v_{i}^{n} dt_{2} + a_{i}^{n} dt dt_{2}$$
(66)

where  $dt = dt_1 + dt_2$ . Hence the difference between the positions calculated by the two approaches is:

$$\bar{x}_{p}^{n+1} - x_{p}^{n+1} = (v_{i}^{n+1} - v_{i-1}^{n+1}) \left[ \frac{x_{i} - x_{p}^{n}}{x_{i} - x_{i-1}} \right] dt_{2} - \left[ a_{i-1}^{n} + \frac{x_{p}^{n} - x_{i-1}}{x_{i} - x_{i-1}} (a_{i}^{n} - a_{i-1}^{n}) \right] dt_{1} dt_{2}$$
 (67)

Dividing both sides of Equation (67) by  $(x_i - x_{i-1})$  gives

$$\frac{\bar{x}_p^{n+1} - x_p^{n+1}}{x_i - x_{i-1}} \approx dt_2 \frac{(v_i^{n+1} - v_{i-1}^{n+1})}{(x_i - x_{i-1})} C - \frac{dt_1 dt_2}{x_i - x_{i-1}} \left[ a_{i-1}^n + \frac{x_p^n - x_{i-1}}{x_i - x_{i-1}} (a_i^n - a_{i-1}^n) \right]$$
(68)

where  $C = [x_i - x_p^n/x_i - x_{i-1}]$  and where  $0 \le C \le 1$ . The term  $\bar{x}_p^{n+1} - x_p^{n+1}/x_i - x_{i-1}$  is the spatial relative error in the position. And as the values of  $(v_i^{n+1} - v_{i-1}^{n+1})$  are O(1) for the case considered here it follows that limiting  $\mathrm{d}t \partial v/\partial x < 0.1$  will control the relative position error on the step, as also suggested in Section 6.2.

#### 8. SPATIAL ERROR ESTIMATION

In evaluating the spatial error there are three main sources of errors: the mass mapping error introduced by Equation (23), the momentum mapping error introduced by Equation (24) and the force mapping error introduced by Equation (26). Before considering these equations it is helpful

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to establish some notations relating to an important result, Theorem 2.3 of Hickernell [28] who proves that for any function  $f(x) \in X^p \equiv [f: df/dx \in L^p([0,1])]$ 

$$\left| \int_{0}^{1} f(y) dy - \frac{1}{N_{p}} \sum_{i=1}^{N_{p}} f(z_{i}) \right| \leq D_{2}(P, N_{p}) \left\| \frac{df}{dx} \right\|_{2}$$
 (69)

where

$$D_2(P, N_p) = \sqrt{\frac{1}{12N_p^2} + \frac{1}{N_p} \sum_{i=1}^{N_p} \left( z_i - \frac{2i - 1}{2N_p} \right)^2}$$
 (70)

 $z_i$  is an ordered set of the points  $x_p \in [0, 1]$ . Although Hickernell proves the result for more general norms, the above result is sufficient for this analysis. It is important to translate Hickernell's result to the sub-intervals used in the MPM method. The constant  $D_2(P, N_p)$  is unchanged except that the points  $(2i-1)/2N_p$  need to be translated to the interval  $I_{i+1}$ . In considering an integral over a domain of width h, Theorem 2.3 then becomes

$$\left| \frac{1}{h_{i+1}} \int_{x_i}^{x_{i+1}} f(y) dy - \frac{1}{N_p^{i+1}} \sum_{i=1}^{N_p^{i+1}} f(x_i) \right| \leq D_2(P, N_p^{i+1}) (h_{i+1})^{1/2} \left\| \frac{df}{dx} \right\|_{2, h_{i+1}}$$
(71)

where

$$\left\| \frac{\mathrm{d}f}{\mathrm{d}x} \right\|_{2,h_{i+1}} = \left[ \int_{x_i}^{x_{i+1}} \left( \frac{\mathrm{d}f}{\mathrm{d}x} \right)^2 \mathrm{d}x \right]^{1/2} \tag{72}$$

and where

$$D_2(P, N_p^{i+1}) = \sqrt{\frac{1}{12(N_p^{i+1})^2} + \frac{1}{N_p^{i+1}h^2} \sum_{i=1}^{N_p^{i+1}} \left( (hz_i + x_i) - \left( x_i + \frac{(2i-1)h}{2N_p^{i+1}} \right) \right)^2}$$
(73)

It should also be noted that from the mean value theorem for integration

$$(h_{i+1})^{1/2} \left[ \int_{x_i}^{x_{i+1}} \left( \frac{\mathrm{d}f}{\mathrm{d}x} \right)^2 \mathrm{d}x \right]^{1/2} = (h_{i+1}) \left| \frac{\mathrm{d}f}{\mathrm{d}x} (\xi) \right|$$
 (74)

for some  $\xi \in I_{i+1}$ . Hence

$$\left| \int_{x_i}^{x_{i+1}} f(y) dy - \frac{h_{i+1}}{N_p^{i+1}} \sum_{i=1}^{N_p^{i+1}} f(x_i) \right| \le D_2(P, N_p^{i+1}) h_{i+1}^2 \left| \frac{df}{dx}(\xi) \right|$$
 (75)

The values of  $D_2(P, N_p^{i+1})$  clearly depend on the point distribution and thus in turn on the problem being solved. Considering the worst case of particles negligible distances apart at the end of an interval it is straightforward to show that

$$\frac{1}{2\sqrt{3}N_p^{i+1}} \leqslant D_2(P, N_p^{i+1}) \leqslant \frac{1}{\sqrt{3}}$$
(76)

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This result has a similar form to the results of Grigoryev *et al.* [6] (as quoted by Brackbill [5]) except that the key difference here lies in the choice of quadrature rule. Vshivkov calculates the error,  $\delta_k$ , in the charge density at node k as computed with the PIC. His result states that

$$\delta_{k} \leqslant \left( \frac{3\rho_{\text{av}}^{2}}{2\rho_{\min}} + h \frac{\rho_{\text{av}}^{2}\rho_{\max}}{6\rho_{\min}^{3}} \left| \frac{\partial \rho}{\partial x} \right|_{\text{max}} \right) \frac{1}{N^{2}} + \frac{h^{2}}{12} \left| \frac{\partial^{2} \rho}{\partial x^{2}} \right|_{\text{max}}$$
(77)

where N is the average number of particles in a cell. In the discussion that follows it is convenient to assume that the meshpoints are evenly spaced, i.e.

$$h = h_{i+1} = h_i \tag{78}$$

## 8.1. Ringing instability

It is also important to remark that, as with any quadrature rule, there exist values of f(x) such that  $f(x_i) = 0$ . For example, if

$$f(x) = \prod_{i=1}^{N_p^i} (x - x_j)$$
 (79)

then the integral approximation is zero and the error is the value of the integral. Furthermore, there are functions that are non-zero at the particle points such as

$$f(x_i) = (-1)^i (80)$$

which in the case of even numbers of mesh points will give a zero contribution to the integral. The problem is made worse by the fact that the quadrature rule is essentially using a piecewise constant approximation to function in forming the integral in the most general case. This loss of information due to quadrature is known as the 'Ringing Instability' and is a well-known feature of particle methods that is attributed to the under-representation of particle data on the grid. Brackbill [25] and MAcNeice [29] explain this instability in terms of Fourier analysis.

# 8.2. Mass projection error

The mass error associated with Equation (23) is denoted by  $E_m^i$  and is defined by

$$E_m^i = \int_{x_{i-1}}^{x_{i+1}} \rho(x) S_i(x) dx - m_i$$
 (81)

where there are  $N_p^j$  points in the interval  $I_j$ . This may be written more explicitly in terms of the points in each interval, by using Equation (15) and (23), as

$$E_{m}^{i} = \int_{x_{i-1}}^{x_{i}} \rho(x) S_{i}(x) dx - \frac{h}{N_{p}^{i}} \sum_{p: x_{p} \in I_{i}} S_{i}(x_{p}) \rho_{p}$$

$$+ \int_{x_{i}}^{x_{i+1}} \rho(x) S_{i}(x) dx - \frac{h}{N_{p}^{i+1}} \sum_{p: x_{p} \in I_{i+1}} S_{i}(x_{p}) \rho_{p}$$
(82)

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The error term is thus composed of two terms each of which is similar to the right side of Equation (75):

$$|E_m^i| \le D_2(P, N_p^i) h^2 \left| \frac{\mathrm{d}(\rho(x)S_i(x))}{\mathrm{d}x} (\xi_1) \right| + D_2(P, N_p^{i+1}) h^2 \left| \frac{\mathrm{d}(\rho(x)S_i(x))}{\mathrm{d}x} (\xi_2) \right| \tag{83}$$

for some  $\xi_1 \in I_i$  and some  $\xi_2 \in I_{i+1}$ . However, as the first derivative of  $S_i(x)$  depends on 1/h, this results in the mass error  $E_m^i$  being first order in h. An approximate  $L_1$  norm of mass projection error is calculated by using the trapezoidal quadrature rule, based upon the true error in the mass at mesh points. The result in Figure 6 shows how the mass projection error grows for different mesh sizes and is first order of mesh size as expected. The errors grow in time in a way that is consistent with first time integration using the forward Euler method.

# 8.3. Momentum projection error

The momentum error associated with Equation (36) is denoted by  $E_P^i$  and is given by a similar expression as the mass error except that terms of the from  $\rho(x)S_i(x)$  are replaced with  $v(x)\rho(x)S_i(x)$ , i.e.

$$|E_P^i| \leq D_2(P, N_p^i) h^2 \left| \frac{\mathrm{d}(\rho(x)v(x)S_i(x))}{\mathrm{d}x} (\xi_1) \right| + D_2(P, N_p^{i+1}) h^2 \left| \frac{\mathrm{d}(\rho(x)v(x)S_i(x))}{\mathrm{d}x} (\xi_2) \right|$$
(84)

for some  $\xi_1 \in I_i$  and some  $\xi_2 \in I_{i+1}$ . It follows that the momentum error is also first order in h. A graph of the momentum projection error is very similar to Figure 6.

#### 8.4. Velocity projection error

The nodal velocity,  $v_i$ , is calculated from the mass and the momentum of the node as in Equation (25). The exact projected velocity is given by

$$v_i^{\text{expro}} = \frac{P_i^{\text{expro}}}{m_i^{\text{expro}}} = \frac{\int S_i(x)\rho(x)v(x)dx}{\int S_i(x)\rho(x)dx}$$
(85)

While the division by an integral containing  $\rho(x)$  may be problematic; the method described above has a number of steps to ensure that at least one particle with mass is in every cell interval.

The error in the velocity projection,  $E_{\text{vproj}}^{i}(t)$ , is defined by:

$$E_{\text{vproj}}^{i}(t) = v_{i}^{\text{expro}} - v_{i} \tag{86}$$

Let  $v(x_i, t)$  be the exact nodal velocity at t, and define the error from projection in the exact value as:

$$E_{v1}^{i}(t) = v(x_i, t) - v_i^{\text{expro}}$$
(87)

Then the overall error in velocity projection may be split into two parts:

$$E_{v}^{i}(t) = v(x_{i}, t) - v_{i} = E_{v1}^{i}(t) + E_{vproj}^{i}(t)$$
(88)

Let

$$\frac{\delta^2 U}{\delta x^2}(x,t) = \rho(x,t)v(x,t) \tag{89}$$

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and

$$\frac{\delta^2 V}{\delta x^2}(x,t) = \rho(x,t) \tag{90}$$

Then the exact velocity is defined by:

$$v(x_i, t) = \frac{h\frac{\delta^2 U}{\delta x^2}(x, t)}{h\frac{\delta^2 V}{\delta x^2}(x, t)}$$
(91)

Using integration by parts, the projection of the velocity satisfies:

$$v_i^{\text{expro}} = \frac{\int S_i(x)\rho(x)v(x)dx}{\int S_i(x)\rho(x)dx} = \frac{\frac{1}{h}(U(x_i - H, t) - 2U(x_i, t) + U(x_i + H, t))}{\frac{1}{h}(V(x_i - H, t) - 2V(x_i, t) + V(x_i + H, t))}$$

Define two projection errors  $E_U^i(t)$  and  $E_V^i(t)$  by

$$E_U^i(t) = h \frac{\delta^2 U}{\delta x^2}(x_i, t) - \int S_i(x) \rho(x) v(x) dx$$
(92)

where using standard finite difference analysis  $E_U^i = O(h^3) + \text{H.O.T}$ , and

$$E_V^i(t) = h \frac{\delta^2 V}{\delta x^2}(x_i, t) - \int S_i(x) \rho(x) dx$$
 (93)

and where  $E_V^i = O(h^3) + \text{H.O.T}$  similarly. The partial projection error  $E_{v1}^i(t)$  is then given by:

$$E_{v1}^{i}(t) = \frac{h \frac{\delta^{2} U}{\delta x^{2}}(x, t)}{h \frac{\delta^{2} V}{\delta x^{2}}(x, t)} - \frac{\int S_{i}(x) \rho(x) v(x) dx}{\int S_{i}(x) \rho(x) dx} = \frac{1}{\int S_{i}(x) \rho(x) dx} (E_{U}^{i} - v(x_{i}, t) E_{V}^{i})$$

As  $E_U^i$  and  $E_V^i$  are third order in h and  $\int S_i(x)\rho(x)\mathrm{d}x$  is first order in h, it follows that  $E_{v1}^i(t)$  is second order in h. The second part of the projection error is defined by

$$E_{\text{vproj}}^{i}(t) = \frac{\int S_{i}(x)\rho(x)v(x)dx}{\int S_{i}(x)\rho(x)dx} - \frac{P_{i}}{m_{i}} = \frac{1}{m_{i}}(E_{p}^{i}(t) - v(x_{i}, t)E_{m}^{i}(t))$$

where

$$E_{p}^{i}(t) = \int_{x_{i-1}}^{x_{i+1}} \rho(x) S_{i}(x) v(x) dx - \frac{h}{N_{p}^{i}} \sum_{p: x_{p} \in I_{i}} S_{i}(x_{p}) \rho_{p} v_{p} - \frac{h}{N_{p}^{i+1}} \sum_{p: x_{p} \in I_{i+1}} S_{i}(x_{p}) \rho_{p} v_{p}$$

Using a Taylor's series expansion of velocity about  $x_i$  gives

$$E_p^i(t) = v(x_i, t)E_m^i(t) + v_x(x_i, t)E_{vp1}^i(t) + \frac{v_{xx}(x_i, t)}{2}E_{vp2}^i(t) + \dots +$$
(94)

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where

$$E_{vpk}^{i} = \int_{x_{i-1}}^{x_{i+1}} S_{i}(x)\rho(x)(x-x_{i})^{k} dx - \frac{h}{N_{p}^{i}} \sum_{p:x_{p} \in I_{i}} \bar{S}_{ip}\rho_{p}(x_{p}-x_{i})^{k}$$

$$-\frac{h}{N_{p}^{i+1}} \sum_{p:x_{p} \in I_{i+1}} \bar{S}_{ip}\rho_{p}(x_{p}-x_{i})^{k}$$
(95)

Therefore

$$E_v^i(t) = E_{v1}^i(t) + \frac{1}{m_i} \left( v_x(x_i, t) E_{vp1}^i(t) + \frac{v_{xx}(x_i, t)}{2} E_{vp2}^i(t) + \cdots \right)$$
(96)

Using Hickernell's result from Equation (71), gives

$$|E_{vpk}^{i}| \leq D_{2}(P, N_{p}^{i})h^{2} \left| \frac{d(\rho(x)S_{i}(x)(x-x_{i})^{k})}{dx} (\xi_{1}) \right| + D_{2}(P, N_{p}^{i+1})h^{2} \left| \frac{d(\rho(x)S_{i}(x)(x-x_{i})^{k})}{dx} (\xi_{2}) \right|$$
(97)

for some  $\xi_1 \in I_i$  and some  $\xi_2 \in I_{i+1}$ . For the lowest-order term k=1 this is second order.

#### 8.5. Acceleration projection error

We define the projection error in acceleration,  $E_a^i$ , is

$$E_a^i = a(x_i, t) - a_i \tag{98}$$

where  $a(x_i, t)$  is the exact acceleration at node  $x_i$  at time t. As for the velocity projection error, the acceleration projection error may be split into two parts:

$$E_a^i = (a(x_i, t) - a_i^{\text{expro}}) + (a_i^{\text{expro}} - a_i) = E_{a1}^i(t) + E_{\text{apro}}^i(t)$$
(99)

where  $a_i^{\text{expro}}$  is the exact nodal acceleration obtained by projecting the exact pressure and density onto the mesh points, and  $a_i$  is the calculated nodal acceleration from (30). The error  $E_{a_1}^i(t)$  may be shown to be second order in h using the same approach as in Equations (85)–(94). The second part of acceleration projection error is:

$$E_{\text{aproj}}^{i}(t) = \frac{\frac{1}{h} \left( \int_{x_{i-1}}^{x_i} p(x) dx - \int_{x_i}^{x_{i+1}} p(x) dx \right)}{\int_{x_{i-1}}^{x_{i+1}} \rho(x) S_i(x) dx} - \frac{1}{N_p^i} \sum_{p: x_p \in I_i} p_p - \frac{1}{N_p^{i+1}} \sum_{p: x_p \in I_{i+1}} p_p$$
(100)

Then

$$E_{\text{aproj}}^{i}(t) = \frac{1}{m_{i}} (E_{F}^{i}(t) - a(x_{i}, t) E_{m}^{i}(t))$$
(101)

where

$$E_F^i = \left(\frac{1}{h} \int_{x_{i-1}}^{x_i} p(x) dx - \frac{1}{N_p^i} \sum_{p: x_p \in I_i} p_p\right) + \left(-\frac{1}{h} \int_{x_i}^{x_{i+1}} p(x) dx + \frac{1}{N_p^{i+1}} \sum_{p: x_p \in I_{i+1}} p_p\right)$$
(102)

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Expanding the values of pressure about  $x_i$  gives

$$\frac{1}{h} \int_{x_{i-1}}^{x_i} p(x) dx - \frac{1}{N_p^i} \sum_{p: x_p \in I_i} p_p = p_x(x_i) \left( \frac{x_i + x_{i-1}}{2} - \frac{1}{N_p^i} \sum_{p: x_p \in I_i} x_p \right) + \frac{p_{xx}(x_i)}{2} \left( \int_{x_{i-1}}^{x_i} \frac{(x - x_i)^2}{h} dx - \frac{h}{N_p^i} \sum_{p: x_p \in I_i} \frac{(x_p - x_i)^2}{h} \right)$$

and similarly for the interval  $[x_i, x_{i+1}]$ . The lowest-order term in the error is then:

$$E_F^i = p_x(x_i) \left( h - \frac{1}{N_p^i} \sum_{p: x_p \in I_i} x_p + \frac{1}{N_p^{i+1}} \sum_{p: x_p \in I_{i+1}} x_p \right) + \text{H.O.T}$$
 (103)

In order to investigate the order of this term it is necessary to consider the evolution of the points that contribute to the calculation of acceleration at the point  $x_i$  at time  $t_n$ . Let means of particle positions and velocities be defined by:

$$\bar{x}_{i+1}^{n}(t) = \frac{1}{N_p^{i+1}} \sum_{p: x_p(t_n) \in I_{i+1}} x_p(t)$$
(104)

$$\bar{v}_{i+1}^{n}(t) = \frac{1}{N_p^{i+1}} \sum_{p: x_p(t_n) \in I_{i+1}} v_p(t)$$
(105)

Furthermore, define

$$\frac{\mathrm{d}\bar{v}_{i}^{n}}{\mathrm{d}x}(t) = \frac{\bar{v}_{i+1}^{n}(t) - \bar{v}_{i+1}^{n}(t)}{\bar{x}_{i+1}^{n}(t) - \bar{x}_{i}^{n}(t)}$$
(106)

From Equations (104), (105) and (107) it follows that

$$\bar{x}_{i+1}^{n}(t_{n+1}) - \bar{x}_{i}^{n}(t_{n+1}) = \left[1 + \Delta t \frac{\mathrm{d}\bar{v}_{i}^{n}}{\mathrm{d}x}(t_{n})\right] (\bar{x}_{i+1}^{n}(t_{n}) - \bar{x}_{i}^{n}(t_{n}))$$
(107)

and hence that the gap between the means may be related back to the initial mesh distribution

$$\bar{x}_{i+1}^{n}(t_{n+1}) - \bar{x}_{i}^{n}(t_{n+1}) = \prod_{i} \left[ 1 + \Delta t \frac{d\bar{v}_{i}^{n}}{dx}(t_{j}) \right] (\bar{x}_{i+1}^{n}(t_{0}) - \bar{x}_{i}^{n}(t_{0}))$$
(108)

Suppose that initially all the points are evenly distributed at time  $t_0$  with spacing  $h_p$ , then

$$(\bar{x}_{i+1}^n(t_0) - \bar{x}_i^n(t_0)) = h_p(N_p^{i+1} + N_p^i)/2$$
(109)

where the interval spacing h is connected to the initial particle spacing  $h_p$  through

$$h = h_p(N_p^0 + 1) \tag{110}$$

where  $N_p^0$  is the total number of points in every interval at  $t_0$ . Hence

$$\bar{x}_{i+1}^{n}(t_{n+1}) - \bar{x}_{i}^{n}(t_{n+1}) = h \prod_{j} \left[ 1 + \Delta t \frac{\mathrm{d}\bar{v}_{i}^{n}}{\mathrm{d}x}(t_{j}) \right] \left[ \frac{N_{p}^{i+1} + N_{p}^{i}}{2(N_{p}^{0} + 1)} \right]$$
(111)

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Using the CFL condition as defined by Equation (46) then gives

$$\bar{x}_{i+1}^{n}(t_{n+1}) - \bar{x}_{i}^{n}(t_{n+1}) = h[1+h \text{ CFL } K] \frac{N_{p}^{i+1} + N_{p}^{i}}{2(N_{p}^{0} + 1)} + \text{H.O.T}$$
 (112)

where

$$K = \sum_{i} \left[ \frac{\mathrm{d}\bar{v}_{i}^{n}}{\mathrm{d}x}(t_{j}) \right] \tag{113}$$

This result shows that the acceleration order may be first order if the local velocity gradients are 'small' if particles are rezoned as to be closer to evenly spaced as in Section 5.3.

## 8.6. Velocity gradient error

The accuracy of the equations used to update energy and density in Section 5.1 depends on the accuracy of the velocity gradient and the velocity gradient at any particle  $x_p \in I_{i+1}$  is defined as:

$$\frac{\delta v}{\delta x}(x_p) = \frac{v_{i+1} - v_i}{x_{i+1} - x_i} - \left(\frac{x_{i+1} + x_i}{2} - x_p\right) \frac{\delta^2 v}{\delta x^2}(x_p) + \text{H.O.T}$$
(114)

The velocity gradient error at particles is rewritten as:

$$E_{VG}^{p} = \frac{E_{v}^{i+1} - E_{v}^{i}}{h} + \frac{\Delta t}{h} \left[ E_{a}^{i+1} - E_{a}^{i} \right] - \left( \frac{x_{i+1} + x_{i}}{2} - x_{p} \right) \frac{\delta^{2} v}{\delta x^{2}} (x_{p})$$
(115)

Thus, the velocity gradient error depends on the first-order interpolation error.

# 9. COMBINING THE ERROR ESTIMATE RESULTS

The density errors at T = 0.2 in the approximate L1-Norm and L2-Norm for different mesh sizes are shown in Table II. We are using same CFL as in Section 6 and the initial number of particles per cell is also eight throughout. The numbers in this table indicate that the density error is order of h in the approximate L1-norm and order of  $h^{1/2}$  in the approximate L2-norm. To understand the orders of these norms, a detailed inspection of the order of accuracy in each part of the spatial domain was made. In the regions around the contact discontinuity and the shock, the maximum

Table II. Density error at T = 0.2 in L1-norm and L2-norm and pointwise maximum error at mesh points.

h	L1-norm	L2-norm	Max. density err. at mesh pts
0.02	0.00161	0.02484	0.1051
0.01	0.00831	0.01587	0.0812
0.005	0.00434	0.01046	0.1139
0.0025	0.00231	0.00759	0.1063
0.00125	0.00136	0.00626	0.1002
0.000625	0.00110	0.00619	0.0989

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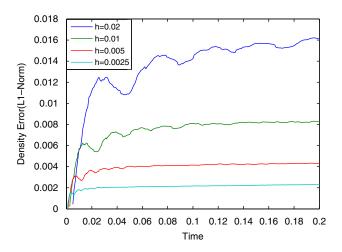


Figure 7. L1-norm of density errors over time for different meshes.

pointwise error does not decrease but the interval over which it occurs is reduced with the mesh spacing h. The approximate L1-norm is  $h|E_{\rm max}|$  while the approximate L2-norm is  $\sqrt{h}|E_{\rm max}|$ , thus, giving rise to the observed orders of convergence. Figure 7 shows the evolution in time of the L1-norm of the density error for different mesh sizes.

#### 10. SUMMARY

In this paper, the accuracy properties of a variant of the MPM are investigated in depth on a well-known test problem in one space dimension. The analysis leads to the same conclusion that the method is order one half to first order in accuracy for a sufficiently small CFL number. The analysis also shows that this accuracy depends on a sufficiently well-behaved point distribution. This point distribution can be verified computationally in a straightforward manner. Computational experiments have been used to show that the observed experiments match the computed experiments. The importance of this analysis is that it provides a way to make a more formal assessment of many of the errors in MPM type methods. This in turn makes it possible to start to consider an analysis of higher space dimensional MPM.

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#### REFERENCES

- 1. Li S, Liu WK. Meshfree particle methods and their applications. Applied Mechanics Review 2002; 54:1-34.
- Sulsky D, Chen Z, Schreyer HL. A particle method for history-dependent materials. Computer Methods in Applied Mechanics and Engineering 1994; 118:179–196.

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- Sulsky D, Zhou S-J, Schreyer HL. Application of a particle-in-cell method to solid mechanics. Computer Physics Communications 1995; 87:236–252.
- Brackbill JU, Ruppel HM. FLIP: a method for adaptively zoned, particle-in-cell calculations of fluid flow in two dimensions. *Journal of Computational Physics* 1986; 65:314–343.
- 5. Brackbill JU. Particle methods. International Journal for Numerical Methods in Fluids 2005; 47:693-705.
- Grigoryev YN, Vshivkov VA, Fedoruk MP. Numerical Particle in Cell Methods Theory and Applications. VSP: Utrecht, Boston, 2002.
- Bardenhagen SG, Kober EM. The generalized interpolation material point method. Computer Modeling in Engineering and Sciences 2004; 5:477–495.
- 8. Brydon AD, Bardenhagen SG, Miller EA, Seidler GT. Simulation of the densification of real open-celled foam microstructures. *Journal of the Mechanics and Physics of Solids* 2005; **53**:2638–2660.
- 9. Henderson TC, McMurtry PA, Smith PJ, Voth GA, Wight CA, Pershing DF. Simulating accidental fires and explosions. *Computing in Science and Engineering* 2000; 2:64–76.
- 10. Parker SG. A component-based architecture for parallel multi-physics PDE simulation. *International Conference on Computational Science (ICCS2002)*. Workshop on PDE Software, 21–24 April 2002, The Netherlands; *Proceedings, Part III MA*, Sloot CJ, Tan K, Dongarra JJ, Hoekstra AG (eds). Lecture Notes in Computer Science, vol. 2331. Springer: Berlin, 2002, GmbH. ISSN: 0302-9743.
- 11. Kim J. MPM Masters Project report unpublished. 2004.
- 12. Burgess D, Sulsky D, Brackbill JU. Mass matrix formulation of the FLIP particle in cell method. *Journal of Computational Physics* 1992; **103**:1–15.
- 13. York AR, Sulsky D, Schreyer HL. Fluid-membrane interaction based on the material point method. *International Journal for Numerical Methods in Engineering* 2000; **48**:901–924.
- Brownlee J, Levesley J, Houston P, Rosswog S. Enhancing SPH using moving least-squares and radial basis functions. *Proceedings of A4A5 (Algorithms for Approximation)*, Chester, U.K., 18–22 July 2005. Springer: Berlin. 2007.
- 15. Ma S, Zhang X, Qiui XM. Comparison study of MPM and SPH in modeling hypervelocity impact problems. *International Journal of Impact Engineering* 2009; **36**:272–282.
- Steffen M, Kirby RM, Berzins M. Analysis and reduction of quadrature errors in the material point method (MPM). *International Journal for Numerical Methods in Engineering* 2008; 76:922–948. DOI:10.1002/nme.2360.
- 17. Steffen M, Wallstedt PC, Guilkey JE, Kirby RM, Berzins M. Examination and analysis of implementation choices within the material point method (MPM). *Computer Modeling in Engineering and Sciences* 2008; **32**:107–127.
- 18. Wallstedt P, Guilkey J. Improved velocity projection for the material point method. Computer Modeling in Engineering and Sciences 2007; 19:223–232.
- 19. Wallstedt PC, Guilkey JE. An evaluation of explicit time integration schemes for use with the generalized interpolation material point method. *Journal of Computational Physics* 2008; **227**:9628–9642.
- 20. Sod GA. A survey of several difference methods for systems of nonlinear hyperbolic conservation laws. *Journal of Computational Physics* 1978; **27**:1–31.
- Leveque RJ. Finite volume methods for hyperbolic problems. Cambridge Texts in Applied Mathematics. Cambridge University Press: Cambridge, 2002.
- 22. Chawla MM, Subramanian R. Regions of absolute stability of explicit Runge Kutta Nystrom methods for y'' = f(x, y, y'). Journal of Computational and Applied Mathematics 1984; 11:259–266.
- Monaghan JJ, Gingold RA. Shock simulation by the particle method SPH. *Journal of Computational Physics* 1983; 52:374–389.
- Monaghan JJ, Pongracic H. Artificial viscosity for particle methods. Applied Numerical Mathematics 1985;
   1:187–194.
- 25. Brackbill JU. The ringing instability in particle in cell calculations of low-speed flow. *Journal of Computational Physics* 1988; **75**:469–492.
- 26. Shampine LF. Local error estimation by doubling. Computing 1985; 4:179-190.
- 27. Ascher UM, Petzold LR. Computer Methods for Ordinary Differential Equations and Differential Algebraic Equations. SIAM: Philadelphia, PA, 1998.
- 28. Hickernell FJ. A generalized discrepancy and quadrature bound. Mathematics of Computation 1998; 67:299-322.
- 29. MAcNeice P. Particle mesh techniques. NASA Contractor Report 4666, Hughes STX, Goddard Space Center, Greenbelt MD, 1995.

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